

Homework #6: Reaction and Diffusion Analysis

1. Reaction and Diffusion in a Spherical Pellet w/ External Mass Transfer Limitations
 - (a) Derive the relationship between dimensionless concentration and position for the case of reaction and diffusion in a spherical catalyst with finite external mass transfer.
 - (b) Plot concentration within the pellet for $\phi = 0.1, 0.2, 0.5, 1, 2, 5, 10$ if $Bi_m = 100$.
 - (c) Plot concentration within the pellet for $\phi = 0.1, 0.2, 0.5, 1, 2, 5, 10$ if $Bi_m = 10$.
 - (d) Plot concentration within the pellet for $\phi = 0.1, 0.2, 0.5, 1, 2, 5, 10$ if $Bi_m = 1$.
 - (e) Plot effectiveness as a function of ϕ , for $Bi_m = 100, 10, 1$.

2. Reaction and diffusion within a Cartesian slab with non-elementary kinetics.

Consider reaction and diffusion within a Cartesian slab following unimolecular reaction following Langmuir-Hinshelwood kinetics,

$$r = \frac{kA}{1 + KA}, \quad D_e \frac{dA^2}{dx^2} = r(A).$$

- (a) Derive the dimensionless differential relationship between concentration and position, assuming steady-state reaction and diffusion.
- (b) Assuming symmetry within the catalyst and negligible external mass transfer resistance, and $p = 2$, $KA_o = 5$, solve for the concentration profile within the pellet. You may use any numerical solver you wish – Matlab, Polymath, or even Excel.
- (c) Using your solution from part (b), calculate the catalyst effectiveness.
- (d) Repeat parts (b,c), if $\phi = 0.1$.

Consider reaction and diffusion within a Cartesian slab following power-law kinetics of order [-1].

- (a) Derive the dimensionless differential relationship between concentration and position, assuming steady-state reaction and diffusion.
- (b) Assuming symmetry within the catalyst and negligible external mass transfer resistance, solve for the concentration profile within the pellet if $\phi = 1$.
- (c) Using your solution from part (b), calculate the catalyst effectiveness.